Mixed flows in closed water pipes A kinetic approach

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French-Chinese Summer Research Institute Project "Stress tensor effects on compressible flows", Morningside Center of Mathematics of the Chinese Academy of Sciences Beijing, 2-23 janvier 2010.





Modelisation: the pressurised and free surface flows model

- The free surface model
- The pressurised model
- The PFS-model : a natural coupling

The kinetic approach

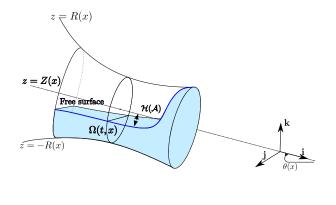
- The Kinetic Formulation
- The kinetic scheme : the case of a non transition point
- The case of a transition point

3 Numerical experiments

4 Conclusion and perspectives



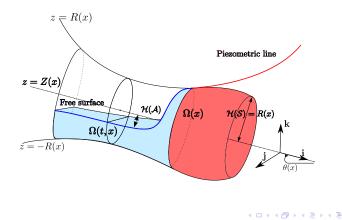
• Free surface (FS) area : only a part of the section is filled.



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What is a transient mixed flow in closed pipes

- Free surface (FS) area : only a part of the section is filled.
- Pressurized (P) area : the section is completely filled.



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a forced pipe



a sewer in Paris



The Orange-Fish Tunnel (in Canada)





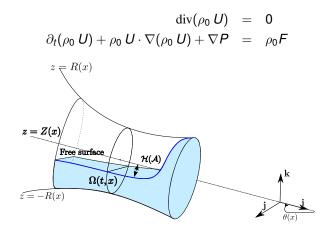
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The domain $\Omega_F(t)$ of the flow at time t: the union of sections $\Omega(t, x)$ orthogonal to some plane curve C lying in $(O, \mathbf{i}, \mathbf{k})$ following main flow axis. $\omega = (x, 0, b(x))$ in the cartesian reference frame $(O, \mathbf{i}, \mathbf{j}, \mathbf{k})$ where \mathbf{k} follows the vertical direction; b(x) is then the elevation of the point $\omega(x, 0, b(x))$ over the plane $(O, \mathbf{i}, \mathbf{j})$

Curvilinear variable defined by:

$$X=\int_{x_0}^x\sqrt{1+(b'(\xi))^2}d\xi$$

where x_0 is an arbitrary abscissa. Y = y and we denote by Z the **B**-coordinate of any fluid particle *M* in the Serret-Frenet reference frame $(\mathbf{T}, \mathbf{N}, \mathbf{B})$ at point $\omega(x, 0, b(x))$.



write the Euler equations in a curvilinear reference frame,

- 2 $\epsilon = H/L$ with *H* (the height) and *L* (the length) and take $\epsilon = 0$ in the Euler curvilinear equations,
- the conservative variables A(t, X): the wet area, Q(t, X) the discharge defined by

$$A(t,X) = \int_{\Omega(t,X)} dY dZ, \quad Q(t,X) = A(t,X)\overline{U}$$

$$\overline{U}(t,X) = \frac{1}{A(t,X)} \int_{\Omega(t,X)} U(t,X) \, dY dZ.$$

(approximation : $\overline{U^2} \approx \overline{U} \overline{U}$ and $\overline{UV} \approx \overline{UV}$.



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$$\begin{cases} \partial_t A + \partial_X Q = 0 \\ \partial_t Q + \partial_X \left(\frac{Q^2}{A} + g I_1(X, A) \cos \theta \right) = g I_2(X, A) \cos \theta - g A \sin \theta \quad (1) \\ -g A \overline{Z}(X, A) (\cos \theta)' \end{cases}$$

$$I_1(X, A) = \int_{-R}^{h} (h - Z) \sigma \, dZ : \text{the hydrostatic pressure term}$$

$$I_2(X, A) = \int_{-R}^{h} (h - Z) \partial_X \sigma \, dZ : \text{the pressure source term}$$

 $\widetilde{p} = \rho_0(h(t, X) - Z) \cos \theta : \text{the hydrostatic pressure.}$ $\overline{Z} = \int_{\Omega(t, X)} Z \, dY \, dZ : \text{the center of mass}$

We add the Manning-Strickler friction term of the form

$$S_f(A, U) = K(A)U|U|.$$



4 E > 4



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$$\partial_t \rho + \operatorname{div}(\rho \mathbf{U}) = \mathbf{0}, \qquad (2$$

$$\partial_t (\rho \mathbf{U}) + \operatorname{div}(\rho \mathbf{U} \otimes \mathbf{U}) + \nabla p = \mathbf{F}, \qquad (3$$

Linearized pressure law:

$$oldsymbol{
ho} = oldsymbol{
ho}_{a} + rac{
ho -
ho_{0}}{eta
ho_{0}}$$
 $oldsymbol{c} = rac{1}{\sqrt{eta
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$$A = \frac{\rho}{\rho_0} S, \ Q = A\overline{U}$$

$$\overline{U}(t,X) = \frac{1}{S(X)} \int_{S(X)} U(t,X) \, dY dZ.$$

Approximation : $\overline{\rho U^2} \approx \rho \overline{U} \overline{U}$ and $\overline{\rho U} \approx \rho \overline{U}$.



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$$\begin{cases} \partial_t(A) + \partial_X(Q) &= 0\\ \partial_t(Q) + \partial_X \left(\frac{Q^2}{A} + c^2 A\right) &= -gA\sin\theta - gA\overline{Z}(X,S)(\cos\theta)' \qquad (4)\\ &+ c^2 A\frac{S'}{S} \end{cases}$$

 $c^2 A$: the pressure term $c^2 A \frac{S'}{S}$: the pressure source term due to geometry changes $g A \overline{Z}(X, S)(\cos \theta)'$: the pressure source term due to the curvature \overline{Z} : the center of mass.

We add the Manning-Strickler friction term of the form

$$S_f(A, U) = K(A)U|U|.$$



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$$\begin{cases} \partial_t(A) + \partial_x(Q) &= 0\\ \partial_t(Q) + \partial_x \left(\frac{Q^2}{A} + p(x, A, S)\right) &= -g A \frac{d}{dx} Z(x) \\ &+ Pr(x, A, S) \\ &- G(x, A, S) \\ &- g A K(x, S) u |u| \end{cases}$$

• $A = \frac{\rho}{\rho_0} S$: wet equivalent area,

- Q = Au: discharge,
- S the physical wet area.

The pressure is $p(x, A, S) = c^2 (A - S) + g I_1(x, S) \cos \theta$.



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• The pressure source term:

$$Pr(x,A,S) = \left(c^2 \left(\frac{A}{S}-1\right)\right) \frac{d}{dx}S + g l_2(x,S) \cos \theta,$$

the z-coordinate of the center of mass term:

$$G(x, A, S) = g A \overline{Z}(x, S) \frac{d}{dx} \cos \theta,$$

the friction term:

$$K(x,S) = rac{1}{K_s^2 R_h(S)^{4/3}}$$

- $K_s > 0$ is the Strickler coefficient,
- $R_h(S)$ is the hydraulic radius.

[[]BEG09] C. Bourdarias, M. Ersoy and S. Gerbi. A model for unsteady mixed flows in non uniform closed water pipes and a well-balanced finite volume scheme. IJFV, 2009.



Mathematical properties

- The PFS system is strictly hyperbolic for A(t, x) > 0.
- For smooth solutions, the mean velocity u = Q/A satisfies

$$\partial_t u + \partial_x \left(\frac{u^2}{2} + c^2 \ln(A/S) + g \mathcal{H}(S) \cos \theta + g Z \right)$$

= $-g \mathcal{K}(x, S) u |u|$

and u = 0 reads: $c^2 \ln(A/S) + g \mathcal{H}(S) \cos \theta + g Z = 0$.

It admits a mathematical entropy

$$E(A, Q, S) = \frac{Q^2}{2A} + c^2 A \ln(A/S) + c^2 S + g \overline{Z}(x, S) \cos \theta + g A Z$$

which satisfies the entropy inequality

$$\partial_t E + \partial_x \left(E \, u + p(x, A, S) \, u \right) = -g \, A \, K(x, S) \, u^2 \, |u| \leqslant 0$$



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With

$$\chi(\omega) = \chi(-\omega) \ge 0 \;,\; \int_{\mathbb{R}} \chi(\omega) d\omega = 1, \int_{\mathbb{R}} \omega^2 \chi(\omega) d\omega = 1 \;,$$



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$$\chi(\omega) = \chi(-\omega) \ge 0 \;,\; \int_{\mathbb{R}} \chi(\omega) d\omega = 1, \int_{\mathbb{R}} \omega^2 \chi(\omega) d\omega = 1 \;,$$

we define the Gibbs equilibrium

$$\mathcal{M}(t, x, \xi) = \frac{A}{c(A)} \chi\left(\frac{\xi - u(t, x)}{c(A)}\right)$$

with

$$c(A) = \sqrt{g \frac{l_1(x, A)}{A} \cos \theta} \text{ in the FS zones and,}$$
$$c(S) = \sqrt{g \frac{l_1(x, S)}{S} \cos \theta + c^2} \text{ in the P zones.}$$



We have the macroscopic-microscopic relations:

$$A = \int_{\mathbb{R}} \mathcal{M}(t, x, \xi) \, d\xi$$
$$Q = \int_{\mathbb{R}} \xi \mathcal{M}(t, x, \xi) \, d\xi$$
$$\frac{Q^2}{A} + Ac(A)^2 = \int_{\mathbb{R}} \xi^2 \mathcal{M}(t, x, \xi) \, d\xi$$



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The Kinetic Formulation

(A, Q) is a strong solution of PFS-System if and only if \mathcal{M} satisfies the kinetic transport equation:

$$\partial_t \mathcal{M} + \xi \cdot \partial_x \mathcal{M} - g \Phi(x, A, S) \partial_{\xi} \mathcal{M} = K(t, x, \xi)$$

for some collision term $K(t, x, \xi)$ which satisfies for a.e. (t, x)

$$\int_{\mathbb{R}} K \, d\xi = 0 \ , \ \int_{\mathbb{R}} \xi \, K d \, \xi = 0$$

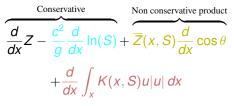
Φ takes into account all the source terms.

[P02] B. Perthame. Kinetic formulation of conservation laws. Oxford University Press. Oxford Lecture Series in Mathematics and its Applications, Vol 21, 2002.



The source terms

• If $A \neq S$, Φ reads:







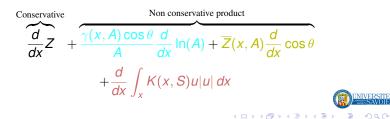
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If ^{A=S}, Φ reads:





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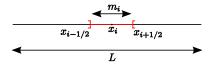
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Geometric terms and unknowns are piecewise constant approximations on the cell m_i at time t_n :

- Geometric terms
 - *S*_{*i*}, cos θ_{*i*}
- Macroscopic unknowns

•
$$\mathbf{W}_i^n = (A_i^n, Q_i^n), \ u_i^n = \frac{Q_i^n}{A_i^n}$$

Microscopic unknown

•
$$\mathcal{M}_i^n(\xi) = \frac{A_i^n}{c_i^n} \chi\left(\frac{\xi - u_i^n}{c_i^n}\right)$$



Consequently Φ_i^n is null on m_i .

Indeed, we have:

•
$$\frac{d}{dx}(\mathbb{1}_{m_i}Z) = 0,$$

•
$$\frac{d}{dx}(\ln(\mathbb{1}_{m_i}S)) = 0,$$

•
$$\frac{d}{dx}(\mathbb{1}_{m_i}\cos\theta) = 0,$$

•
$$\frac{d}{dx}\int_x K(x,S)u|u|\,dx = 0$$

[PS01] B. Perthame and C. Simeoni. A kinetic scheme for the Saint-Venant system with a source term. Calcolo, Vol 38(4) 201-231, 2001



4 E > 4

Neglecting the collision term, the transport equation reads on $[t_n, t_{n+1}] \times m_i$:

$$\frac{\partial}{\partial t}\mathbf{f} + \boldsymbol{\xi} \cdot \frac{\partial}{\partial x}\mathbf{f} = \mathbf{0}$$

with $f(t_n, x, \xi) = \mathcal{M}_i^n(\xi)$ for $x \in m_i$ and thus it is discretised on m_i as:

$$f_{i}^{n+1}(\xi) = \mathcal{M}_{i}^{n}(\xi) + \frac{\Delta t^{n}}{\Delta x} \xi \left(\mathcal{M}_{i+\frac{1}{2}}^{-}(\xi) - \mathcal{M}_{i-\frac{1}{2}}^{+}(\xi) \right) ,$$



Although f_i^{n+1} is not a Gibbs equilibrium, we have :

$$\mathbf{W}_{i}^{n+1} = \begin{pmatrix} A_{i}^{n+1} \\ Q_{i}^{n+1} \end{pmatrix} \stackrel{\text{def}}{\coloneqq} \int_{\mathbb{R}} \begin{pmatrix} 1 \\ \xi \end{pmatrix} f_{i}^{n+1}(\xi) d\xi$$

 $\longrightarrow \mathcal{M}_i^{n+1}$ defined without using the collision kernel : it is a way to perform all collisions at once



Finally the kinetic scheme reads:

$$\mathbf{W}_{i}^{n+1} = \mathbf{W}_{i}^{n} + \frac{\Delta t^{n}}{\Delta x} \left(F_{i+\frac{1}{2}}^{-} - F_{i-\frac{1}{2}}^{+} \right)$$

with the interface fluxes

$$F_{i+\frac{1}{2}}^{\pm} = \int_{\mathbb{R}} \xi \begin{pmatrix} 1 \\ \xi \end{pmatrix} \mathcal{M}_{i+\frac{1}{2}}^{\pm}(\xi) \, d\xi$$

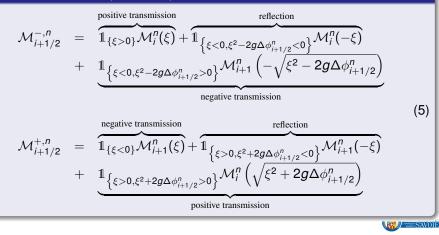
where the microscopic fluxes are defined following e.g. [BEG09b, PS01]:

[BEG09b] C. Bourdarias and M. Ersoy and S. Gerbi. A kinetic scheme for pressurised flows in non uniform closed water pipes. Monografias de la Real Academia de Ciencias de Zaragoza, Vol 31 1–20, 2009.



The microscopic fluxes are given by

Expression of $\mathcal{M}_{i+1/2}^{-,n}$, $\mathcal{M}_{i+1/2}^{+,n}$



The potential barrer and the physical interpretation

The potential barrier $\Delta \phi_{i\pm 1/2}^n$ has the following expression:

$$\Delta \phi_{i+1/2}^{n} = \begin{cases} \left[\left[Z + \int_{x} K(x, S) u | u | dx \right] \right]_{i+1/2} \\ - \frac{c^{2}}{g} \left[\left[\ln(S) \right] \right]_{i+1/2} \\ + \left[\left[\cos \theta \right] \right]_{i+1/2} \int_{0}^{1} \overline{Z}(s, \psi_{S}(s)) ds & \text{if } E_{i}^{n} = 1 \\ \left[\left[Z + \int_{x} K(x, A) u | u | dx \right] \right]_{i+1/2} \\ - \left[\left[A \right] \right]_{i+1/2} \int_{0}^{1} \frac{\gamma(s, \psi_{A}(s))}{\psi_{A}(s)} (\psi_{\cos \theta}) ds \\ + \left[\left[\cos \theta \right] \right]_{i+1/2} \int_{0}^{1} \overline{Z}(s, \psi_{A}(s)) ds & \text{if } E_{i}^{n} = 0 \end{cases}$$

where ψ_A (resp. ψ_S) is the straight lines path connecting the left state A_i (resp. S_i) to the right one A_{i+1} (resp. S_{i+1}).

- be reflected: this means that the particle has not enough kinetic energy $\xi^2/2$ to overpass the potential barrier (reflection in (5)),
- overpass the potential barrier with a positive speed (positive transmission in (5)),
- overpass the potential barrier with a negative speed (negative transmission in (5)).



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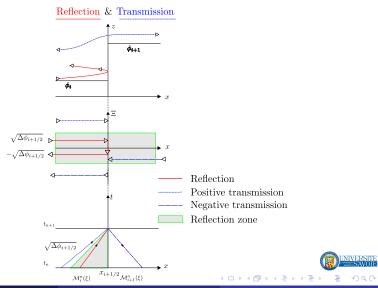


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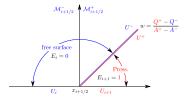


Figure: Free Surface / Pressurised

We have 5 unknowns : U^+ , U^- , w. 5 equations :



- 2 relations to compute $\mathcal{M}_{i+1/2}^{+,n}$
- Conservation of energy

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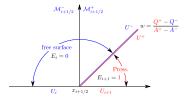


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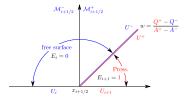


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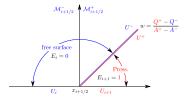
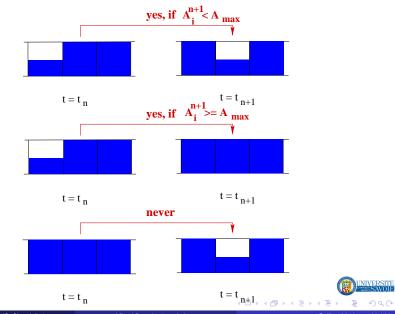


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[ABP00] E. Audusse and M-0. Bristeau and B. Perthame. Kinetic schemes for Saint-Venant equations with source terms on unstructured grids. INRIA Report RR3989, 2000.

$$\chi(\omega) = \frac{1}{2\sqrt{3}}\mathbb{1}_{\left[-\sqrt{3},\sqrt{3}\right]}(\omega)$$

We assume a CFL condition. Then

Properties of the numerical scheme

- The kinetic scheme keeps the wetted area Aⁿ positive,
- Drying and flooding are treated.



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A water-hammer test



An injection test



A double dam break





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Conclusion

- Easy implementation of source terms
- Very good agreement for uniform case
- Drying and flooding area are computed

Perspective

- Air entrainment treated as a bilayer fluid flow (in progress).
- Diphasic approach to take into account air entrapment, evaporation/condensation and cavitation.
- Network of pipes to model town sewers.



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Thank you for your attention



S. Gerbi (LAMA, UdS, Chambéry)

Mixed flows in closed pipes

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